



Adsorption behavior of atmospheric CO₂ with/without water vapor on CeO₂ surface

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ABSTRACT

The significance of investigations into CO₂ adsorption from the air has been steadily on the rise in recent years. CeO₂ is known as an effective catalyst for CO₂ transformation and adsorbent of CO₂, however, the study on the adsorption of low concentrations of CO₂ on CeO₂ and the effect of water vapor on the adsorption of CO₂ on CeO₂ is very limited. Herein, the adsorption behavior of low concentration of CO₂, particularly atmospheric CO₂ (0.04 vol%), on CeO₂ and the effect of water vapor on the CO₂ adsorption were investigated by *in situ* FT-IR, mass spectroscopies, and DFT calculations. Low concentrations of CO₂ can be effectively adsorbed on CeO₂, and typical four CO₂ adspecies such as bidentate carbonate, hydrogen carbonate, monodentate carbonate, and polydentate carbonate were formed on CeO₂. The CO₂ adsorption amount on CeO₂ was increased by 20% by the presence of water vapor compared with that in the absence of water vapor. Based on FT-IR analyses and DFT calculations, the adsorption strength of CO₂ is comparable to that of water on CeO₂, and the water adspecies will assist the adsorption of CO₂ via hydrogen bonding, leading to the increase of CO₂ adsorption amount.

1. Introduction

Global warming is an urgent issue all over the world, which causes various problems such as dangerous weather events, drought, rising sea levels, melting glaciers, and so on, and these problems will become a threat to human life and communities [1,2]. CO₂ is a main gas of greenhouse effect gases, and hence the development of new methods for decreasing the CO₂ concentration in the air is highly required. Various CO₂ adsorption methods such as physical and chemical adsorption methods using amine-based adsorbents and porous materials and so on have been intensively developed and commercialized [3,4]. Direct air capture (DAC) is also a highly promising solution for extracting carbon dioxide directly from the atmosphere because the technology is independent of the origin of CO₂ emissions and enables strategic placement of capture facilities in areas with optimal energy economics or robust access to renewable energy [4–6]. The development of CO₂ transformation methods is also of great importance as well as the CO₂ capture technologies. One of the promising methods is the chemical transformation of CO₂ into valuable chemicals [7–11] because the chemical transformation can fix CO₂ into chemicals and contribute to carbon recycling. The combination of these methods is called carbon dioxide

capture and utilization (CCU), where CO₂ capture including CO₂ adsorption and desorption, and CO₂ transformation to valuable chemicals are typically consecutive processes. However, the separation and purification in the CO₂ capture process are usually energy-consuming because the desorption of the captured CO₂ generally requires heating, namely large energy [11]. Recently, integrated capture and conversion of CO₂ by using materials with both functions of CO₂ adsorption ability and catalysis have attracted attention, and various homogeneous and heterogeneous catalyst systems have been developed. Main researches with homogeneous catalysts are as follows: The combination of CO₂ capture and hydrogenation to methanol using complex catalysts, mainly Ru complexes, and the combination of CO₂ capture and hydrogenation to formic acid derivatives using Rh, Ru, Ir complexes, and so on [12]. Considering the reusability and stability of catalysts, heterogeneous catalysts are preferable to homogeneous ones. As for heterogeneous catalysts, basic metal oxides have been reported to be effective for the capture of CO₂ due to the base property, and the combination of metal species such as Ni, Ru, Rh, Pt, and Cu with the basic metal oxides such as CaO, MgO and Na₂CO₃ are used for the CO₂ capture and conversions such as hydrogenation to methane, reverse water-gas shift reaction, reforming with alkanes and hydrogenation to methanol [13–19].

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However, the report on only metal oxides having both functions of the CO₂ capture and conversion is very limited, and to our best knowledge, Fe₅Co₅Mg₁₀CaO is only the metal oxide, which is effective for CO₂ capture and reverse water-gas shift reaction at 923 K to show 90% conversion of CO₂ and high selectivity (>99%) to CO [20]. Therefore, the development of effective solid catalyst systems having both functions of CO₂ capture and transformation is highly required.

Cerium oxide (CeO₂) has unique acid/base and redox properties and is often used as catalysts or catalyst supports for various gas-phase and liquid-phase reactions [21–30]. It is well-known that CeO₂ is an effective heterogeneous catalyst for the conversion of CO₂ with alcohols and/or amines, and the corresponding carbonate derivatives such as organic (poly)carbonates [31–48], carbamates [49–61] and ureas [52,53] are produced in high yields with high-pressure and/or high-concentration CO₂. Recently, Tomishige and co-workers reported that CeO₂ catalyzed the conversion of ethylenediamine carbamate prepared from CO₂ and ethylenediamine to ethylene urea in high yields in the absence of external CO₂ [54–56]. These results indicate that CeO₂ can catalyze the carboxylation of amines under a low CO₂ pressure or a low concentration of CO₂, which presents the possibility of CO₂ transformations under a low concentration of CO₂ or without additional CO₂ over a CeO₂ catalyst. In the transformation of CO₂ to carbonate derivatives over CeO₂-based catalysts, the acid-base bifunctionality of CeO₂ was generally reported to be responsible for the activation of CO₂ and methanol and/or amines [21,26,28,29,57,58], and based on the correlation between the basic site amount and CO₂ formation rate (or amount) in the synthesis of organic carbonates, the acid-base site was proposed to be the main active site of CeO₂-based catalysts [44,59–62]. On the other hand, the oxygen vacancy site of CeO₂ was reported to be the active site of CO₂ mainly in the reductive transformation of CO₂, such as CO₂ methanation, CO₂ hydrogenation, water-gas shift reaction, dry reforming, and so on [63,64], which will be related to the redox property of CeO₂. Recently, the oxygen vacancy site was reported to be effective for the activation of CO₂ also in the organic carbonate syntheses based on XANES analyses [65]. DFT calculation on CO₂ adsorption on CeO₂ (111), which is the most stable facet, reported that CO₂ can be adsorbed and activated by the basic site or acid-based site as monodentate and bidentate CO₂ adspecies, which are the main adspecies of CO₂ on CeO₂, leading to the bending of the C–O–C bond and the elongation of the C–O bond [66]. The activation mode was supported by FT-IR and XPS analyses [67], and the bending of C–O–C and the length of the C–O bond are indexes for the activation of CO₂.

On the other hand, CeO₂ is a promising adsorbent of CO₂, and the adsorption behavior of CO₂ on CeO₂ has been studied by various methods such as FT-IR, XAS, XPS, DFT-calculations, and so on [66–79]. Particularly, *in-situ* FT-IR analysis is a powerful tool to directly measure the CO₂ adspecies on CeO₂, and four main CO₂ adspecies such as bidentate carbonate, hydrogen carbonate, monodentate carbonate and polydentate carbonate adspecies are proposed to be formed on CeO₂ under pure CO₂ gas flow [59,60]. After the study, the adsorption amount of CO₂ over typical metal oxides such as CeO₂, SiO₂, ZrO₂, and γ -Al₂O₃ was compared by Nomura and co-workers [77], which shows that CeO₂ has a larger CO₂ adsorption amount ($\sim 1 \mu\text{mol m}^{-2}$, $\sim 130 \text{ mmol kg}^{-1}$) than the other metal oxides and that the hydrogen carbonates are weekly adsorbed on CeO₂ based on FT-IR analysis. These results suggest that CeO₂ is a promising adsorbent of CO₂. If CeO₂ is used for the integrated capture and conversion of CO₂, particularly CO₂ in the air, the CO₂ adsorption amount over CeO₂ from the air and the adsorption state of CO₂ including adsorption/desorption temperatures of CO₂ are important information. Moreover, considering that the air contains water vapor, the effect of water vapor is also of great importance because water vapor can affect the CO₂ adsorption on CeO₂. However, reports on the CO₂ adsorption state over CeO₂ in a low-concentration CO₂ (preferably 0.04 vol%) and the effect of water vapor on the CO₂ adsorption state are very limited, and to our best knowledge, there are two reports by Yoshikawa and co-workers [78,79]. They investigated

the effect of water ($\sim 3 \text{ vol}\%$) on CO₂ adsorption over CeO₂ comparing the CO₂ adsorption amount and CO₂ desorption temperature with/without water vapor by *in-situ* FT-IR and mass spectroscopies with $\sim 10 \text{ vol}\%$ CO₂ gas flow [78]. The adsorbed water has little effect on CO₂ adsorption amount on CeO₂ but the desorption of CO₂ adspecies on CeO₂ in the presence of water was easier than that in the absence of water. In the other report [79], they compared the same parameters (CO₂ adsorption amount and CO₂ desorption temperature) with/without water by the same methods with a low CO₂ concentration of CO₂ (0.04 vol%). The CO₂ adsorption amount on the CeO₂ pre-treated by water vapor is a little lower than that without water vapor pretreatment. In addition, the desorption temperature of CO₂ adspecies is higher than that without the water vapor pretreatment. These results are contrary to those of the previous report [78], although the CO₂ concentrations used in these experiments are different ($\sim 10 \text{ vol}\%$ [78] and 0.04 vol% [79]).

As above, the behavior of CO₂ adsorption and desorption on CeO₂ in the presence/absence of water vapor seems to be complicated and remains elusive. In addition, the CO₂ adsorption state on CeO₂ in the presence of water vapor was not discussed in these reports. Therefore, the adsorption behavior and state of CO₂ on CeO₂ under a low concentration of CO₂ with/without water and also the effect of water on CO₂ adsorption on CeO₂ are open to argument. Herein, the adsorption behavior of low concentrations of CO₂ on CeO₂ was investigated by *in-situ* FT-IR, mass spectroscopy, and DFT calculations. In addition, the effect of water vapor on the adsorption of CO₂ on CeO₂ was studied.

2. Experimental

2.1. Preparation of metal oxides

CeO₂ samples were prepared by calcining CeO₂ (CeO₂-HS, DAIICHI KIGENSO KAGAKU KOGYO CO., LTD.) at 873 K for 3 h in air.

2.2. Reagent

5 vol% CO₂/He (standard gas, TAIYO NIPPON SANSO CORP), 0.1 vol% CO₂/He (standard gas, TAIYO NIPPON SANSO CORP), He (G1, TAIYO NIPPON SANSO CORP.) and 5 vol% NH₃/He (standard gas, TAIYO NIPPON SANSO CORP) were used by FT-IR, CO₂ and NH₃-TPD and breakthrough measurements. Water vapor ratio in the mixture gas for FT-IR measurement was adjusted by mixing some introducing gas and He gas passing or not passing through distilled water in some proportion. The water vapor ratio for TPD and breakthrough measurement was adjusted by condensing at a controlled temperature introduced gas passing through distilled water.

2.3. Characterization methods

Specific surface areas of metal oxides were measured with BELSORP MINI X (MicrotracBEL Corporation) by using BET method.

CO₂- and NH₃-temperature-programmed desorption (CO₂- and NH₃-TPD) was carried out by BELCAT II + BELL MASS (MicrotracBEL Corporation) with a cryo cooling system. The samples ($\sim 0.1 \text{ g}$) were set in a quartz cell. Before the measurement, the samples were pretreated as follows: the quartz cell including the sample was heated from room temperature to 873 K (pre-treatment temperature) at a rate of 10 K/min under the mixture of He and O₂ (He: 50 mL/min and O₂ 10 mL/min) and then held at 873 K for 10 min.

X-ray diffraction (XRD) patterns were recorded using MiniFlex 600 (Rigaku Corporation) with Cu K α (40 kV, 15 mA) radiation, and the measurement was conducted with samples in air.

2.4. FT-IR measurement

The sample disks ($\phi 20$), which were prepared by using a tablet molder and hydraulic press (20 MPa, 30 s), were located in the *in-situ*

quartz cell with CaF windows and gas lines. The FT-IR spectra were recorded at 4 cm^{-1} resolution in the range from 1000 to 4000 cm^{-1} by FT/IR-6700 (JASCO Corporation) with a deuterated L-alanine triglycine sulphate (DLATGS) detector. CeO_2 was pre-treated at 873 K for 10 min under the mixture of He (30 mL/min) and O_2 (7.5 mL/min) in the cell. The heating rate was 10 K/min. Each FT-IR spectrum was recorded at room temperature under the mixed gas (total flow rate: 30 mL/min). The mixed gas is composed of He (base gas), CO_2 (0, 0.04, 0.1, 1.0, 5.0 vol%), and vapor (0, 0.03, 0.3 vol%). The gases in the measurement system were replaced by He at room temperature under 30 mL/min He for 60 min. The desorption behavior of the CO_2 adspecies on metal oxide was measured by heating the sample cell from room temperature to 873 K under 30 mL/min He. FT-IR spectra are shown as the difference spectra from the spectrum after the pre-treatment unless otherwise noted.

2.5. Quantitative evaluation of adsorbed molecules

Breakthrough measurements were performed by BELCAT II + BEL MASS (MicrotracBEL Corporation) to quantitatively evaluate the equilibrium adsorption amount of CO_2 and water on each sample. A mixed gas containing He (a base gas) and adsorbates (CO_2 or water) was introduced into the sample, and the change in the amount of the adsorbates in the gas passing through the sample was measured as a function of time. For the breakthrough measurements, samples were granulated into 100–150 μm particles, and they were located in the measurement cell (Fig. S1 (I)). Gas was introduced into the measurement cell, and the outlet gas was measured by mass spectroscopy. This experiment was carried out by the following four steps. (1) Pre-treatment: The measurement cell including samples was heated from room temperature to 873 K at the rate of 10 K/min and maintained at 873 K for 10 min under He (50 mL/min) and O_2 (10 mL/min). The cell was cooled down to room temperature under the mixture of He (50 mL/min) and O_2 (10 mL/min). (2) Main step 1 (investigation of mass intensity at saturation): The mixed gas (total flow rate: 30 mL/min) with 0.04, 0.1, 1.0, and 5.0 vol% CO_2/He with or without 0.85 and 1.6 vol% water vapor was introduced to the line 1 at room temperature until saturation of the MASS intensity of CO_2 and water vapor. The gases passing through the line 1 were analyzed by BEL MASS (Fig. S1 (II) connection 1). (3) Main step 2 (breakthrough curve measurement): The mixed gas (total flow rate: 30 mL/min) with 0.04, 0.1, 1.0, and 5.0 vol% CO_2/He with or without 0.85 and 1.6 vol% water vapor was introduced to the measurement cell at room temperature for 30, 120 or 360 min. The gases passing through the sample cell were analyzed by BEL MASS (Fig. S1 (II) connection 2). (4) Desorption: The sample cell was heated from room temperature to 873 K at the rate of 10 K/min and maintained at 873 K for 10 min under He (30 mL/min). And it was cooled down to room temperature under He (30 mL/min). The equilibrium adsorption amount of CO_2 was estimated by the breakthrough curve (Fig. S1). For example, S in Fig. S1 (III) corresponds to the equilibrium adsorption amount of introduced gas. The amounts of stably adsorbed CO_2 were calculated by CO_2 -TPD measurements. The humidity of the introducing gas was regulated by changing the temperature of the test tube equipped with a water bubbler at the range of 278–283 K. In the above (1) ~ (3) procedures, the gas lines were heated at 373 K.

In addition, the sequential adsorption of CO_2 and water vapor on the metal oxide samples was conducted with a similar method as shown in the above four steps except for step (4) to observe the behavior of CO_2 adspecies by water vapor introduction. In step (I), pre-treatment was carried out with the same method as shown in the above steps. In step (II), CO_2 was first introduced into the sample. In step (III), water vapor was introduced into the sample with CO_2 adspecies, and the other steps are the same.

3. Results and discussions

3.1. Characterization of metal oxide samples

The CeO_2 sample was characterized by BET surface area, XRD, and CO_2 - and NH_3 -TPD. The specific surface area of CeO_2 was $91\text{ m}^2/\text{g}$. The results of XRD and CO_2 - and NH_3 -TPD are shown in Figs. S2 and S3. The base site amount is estimated to be 0.149 mmol g^{-1} ($0.0016\text{ mmol m}^{-2}$) and the acid site amount is done to be 0.169 mmol g^{-1} (0.0019 m^{-2}). CeO_2 has a fluorite structure, and the average particle size is estimated to be 9.9 nm by XRD analysis.

3.2. The adsorption state of CO_2 on CeO_2 at low CO_2 concentration and the dependence of CO_2 concentrations on the CO_2 adsorption on CeO_2

At first, CO_2 adspecies on CeO_2 were measured by FT-IR using mixed gases composed of various concentrations of CO_2 (0.04, 0.1, 1, 5 vol%) and He (base gas). Fig. 1 shows the spectra of CO_2 adspecies on CeO_2 under each CO_2 concentration. The raw spectra of Fig. 1 (I) are shown in Fig. S4 and those of Fig. 1 (III) and (IV) are shown in Fig. S5. Fig. 1 (I) shows the FT-IR spectra at the range of $1000\text{--}1800\text{ cm}^{-1}$, which is the fingerprint region of the CO_2 adspecies. Main signals were observed at $1000\text{--}1070$, 1217, 1293, 1365, 1399, 1465, 1504, 1572, 1583, and 1599 cm^{-1} when 0.04 vol% and 0.1 vol% CO_2/He were introduced. When 1 vol% and 5 vol% CO_2/He were introduced, the signal at 1413 cm^{-1} was also clearly observed in addition to the above signals. According to the previous report on CO_2 adspecies on CeO_2 by Lavalley and co-workers [70] (Fig. 1 (II) and Table S1), the assignment of these signals are as follows: The signals at 1293 and 1572 cm^{-1} are assignable to bidentate carbonate adspecies on CeO_2 . The signals at 1465 cm^{-1} and 1365 cm^{-1} are assignable to polydentate carbonate adspecies on CeO_2 . The signals at 1504 cm^{-1} and 1365 cm^{-1} are assigned to monodentate carbonate adspecies on CeO_2 , respectively. The signals at 1217, 1399 and 1583 cm^{-1} and those at 1217, 1413 and 1599 cm^{-1} are assignable to two similar hydrogen carbonate adspecies [70]. The former hydrogen carbonate adspecies are observed in all the CO_2 concentrations and strongly adsorbed on CeO_2 . The latter hydrogen carbonate adspecies are clearly observed under 1 and 5 vol% CO_2/He and weakly adsorbed on CeO_2 .

Fig. 1 (III) and (IV) show the spectra of CO_2 adspecies on CeO_2 at different introduction times in the ranges of $1000\text{--}1800\text{ cm}^{-1}$ and $3500\text{--}3800\text{ cm}^{-1}$ under 0.1 vol% CO_2/He , respectively. The spectra in the range of $3500\text{--}3800\text{ cm}^{-1}$ mainly show the stretching vibrations of hydroxy groups. Main positive signals were observed at 3618 and 3657 cm^{-1} and negative signals were observed at 3669, 3688, and 3716 cm^{-1} , and these signals can be assigned as follows [70]: The positive signal at 3618 cm^{-1} is assignable to $\nu(\text{OH})$ of the hydrogen carbonate adspecies on CeO_2 and that at 3657 cm^{-1} is assignable to $\nu(\text{OH})$ of bridged hydroxy groups. The negative signal at 3669 cm^{-1} is also assignable to $\nu(\text{OH})$ of bridged hydroxyl groups on the CeO_2 surface, that at 3688 cm^{-1} is assignable to $\nu(\text{OH})$ of non-dissociated adsorbed water and that at 3716 cm^{-1} is assignable to $\nu(\text{OH})$ of on-top hydroxy groups on CeO_2 . The positive signal at 3657 cm^{-1} and negative one at 3669 cm^{-1} (Fig. 1 (IV)), which are due to the bridged hydroxy group, are produced by the state change of the bridged hydroxy groups, which can be also seen by the raw spectra of Fig. 1 (IV) (Fig. S5 (III)). The signal at 3660 cm^{-1} is assignable to $\nu(\text{OH})$ of bridged hydroxy groups and shifted from 3660 cm^{-1} to 3658 cm^{-1} with the time. The signal areas around 3660 cm^{-1} are similar (Fig. S6) all the time. These results suggest that bridged hydroxy groups do not react with CO_2 . On the other hand, the intensity of the signal at 3618 cm^{-1} , which is assignable to hydrogen carbonate adspecies, increased and those at 3716 cm^{-1} and 3688 cm^{-1} decreased with time. Considering the signal at 3688 cm^{-1} is attributed to water adspecies, on-top hydroxy groups (observed at 3716 cm^{-1}) react with CO_2 to form the hydrogen carbonate adspecies (Fig. 2). As above, with even low concentrations of CO_2 (0.04 and 0.1 vol% CO_2), similar

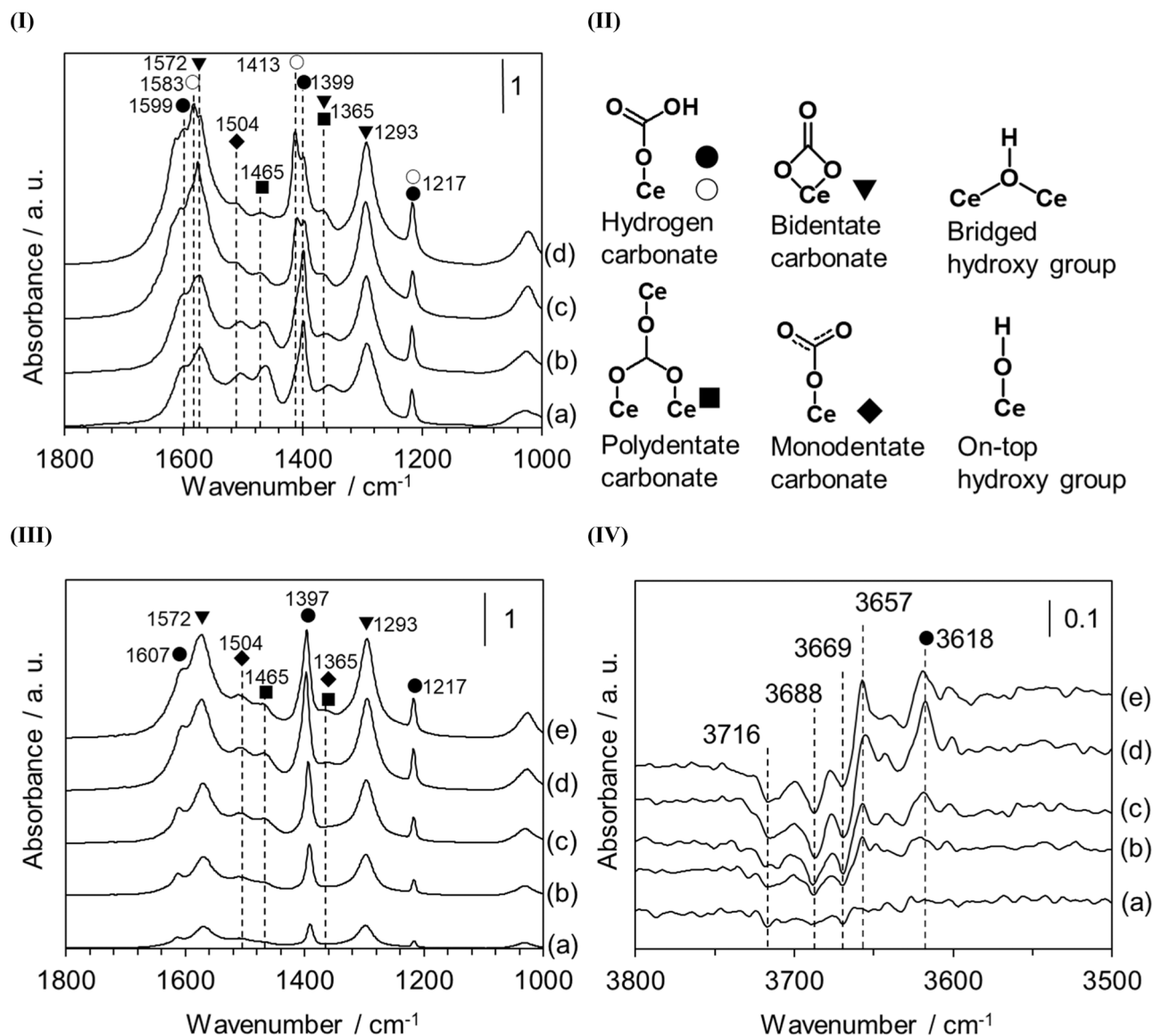


Fig. 1. FT-IR spectra of CO₂ adspecies on CeO₂ at 120 min after introduction of each CO₂ concentration. (I) The spectra at the range of 1000–1800 cm⁻¹ after the introduction of 0.04 vol% CO₂ (a), 0.1 vol% CO₂ (b), 1.0 vol% CO₂ (c), and 5.0 vol% CO₂ (d) for 120 min (II) Images of CO₂ adspecies on CeO₂. (III) The spectra at the range of 1000–1800 cm⁻¹ after the introduction of 0.1 vol% CO₂ for 10 min (a), 20 min (b), 30 min (c), 60 min (d), and 120 min (e). (IV) The spectra at the range of 3500–3800 cm⁻¹ at the conditions of (III). Measurement conditions: CeO₂ 60 mg, disk size φ 20, rt, gas flow rate (CO₂ + He) 30 mL/min.

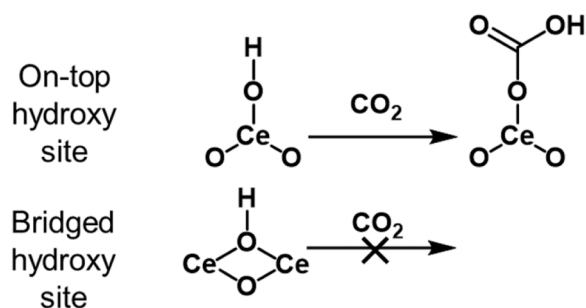


Fig. 2. Image of formation of hydrogen carbonate adspecies from CO₂ and OH adspecies on CeO₂.

CO₂ adspecies to the case of high CO₂ concentrations are formed on CeO₂.

Next, the efficiency of CO₂ adsorption on CeO₂ was evaluated with

various concentrations of CO₂. The signal area of 1200–1800 cm⁻¹, which is due to CO₂ adspecies, was plotted as a function of the time (Fig. 3 (I)). The signal area corresponds to the integrated area as shown in Fig. S7 as an example. The signal area increased with time and leveled off at longer times, suggesting that CO₂ adsorption is saturated on CeO₂. The saturation is faster at higher CO₂ concentrations, which is due to the introduction of large CO₂ amounts per time at high CO₂ concentrations. Fig. 3 (II) shows the signal area as a function of the CO₂ introduced amount. In the range of 0–0.01 mmol CO₂ introduced amount, the signal areas at the same CO₂ introduced amount are higher at the concentration of 0.04 vol% and 0.1 vol% than those at the concentrations of 1 vol% and 5 vol%. These results indicated that low concentrations of CO₂ (0.04 or 0.1 vol%) can be effectively adsorbed on the CeO₂ surface.

Moreover, the breakthrough measurement of CO₂ adsorption on CeO₂ was conducted to investigate the efficiency of CO₂ adsorption. The detailed method is shown in the experimental and Fig. S1. The breakthrough curve with 0.04 vol% (400 ppm) CO₂/He is shown in Fig. 4. The CO₂ concentration of the gas passed through the measurement cell including 1.0 g CeO₂, which is calculated from *M/Z* = 44 intensity, is

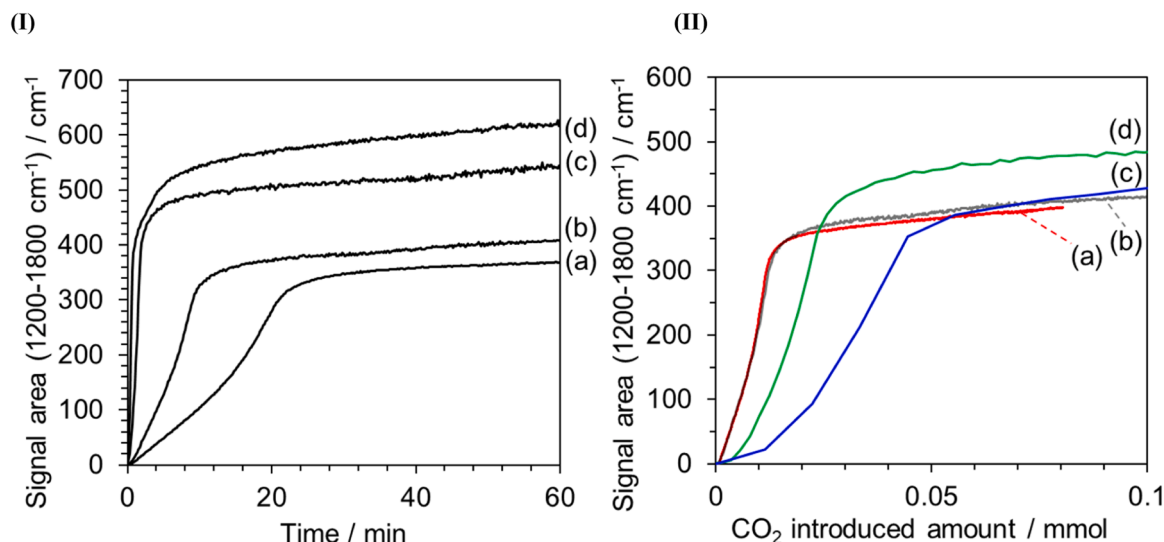


Fig. 3. The change of the signal area (1200–1800 cm⁻¹) of CO₂ adspecies on CeO₂ under different CO₂ concentrations. (I) The signal area (1200–1800 cm⁻¹) as a function of the time. (II) The signal area (1200–1800 cm⁻¹) as a function of introduced CO₂ amount. (a) 0.04 vol% CO₂, (b) 0.1 vol% CO₂, (c) 1 vol% CO₂, and (d) 5 vol% CO₂. Measurement conditions: CeO₂ 60 mg, disk size ϕ 20, rt, gas flow rate (CO₂ + He) 30 mL/min.

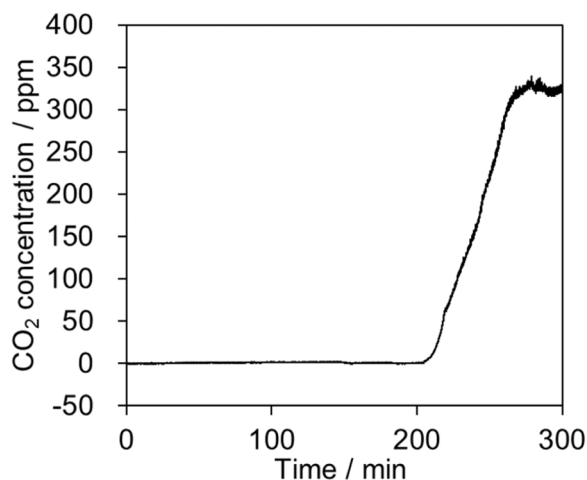


Fig. 4. Breakthrough curve of the introduction of 0.04 vol% CO₂/He into CeO₂. Measurement conditions: CeO₂ 1.0 g (100–150 μm grain), adsorption temperature rt, gas flow rate 30 mL/min.

plotted as a function of the time. The signal of $M/Z = 44$ was hardly detected until about 200 min (the detection limitation: CO₂ concentration < 3 ppm), suggesting that 99% and more of CO₂ was adsorbed on CeO₂ even at the low CO₂ concentration of 0.04 vol% (400 ppm). The equilibrium adsorption amount of CO₂ on CeO₂ was calculated by subtracting the detected CO₂ amount by mass spectrometer from the CO₂ introduced amount (Fig. S1(III), red colored area). The equilibrium CO₂ adsorption amount in the case of 0.04 vol% CO₂ is calculated to be 0.13 mmol g⁻¹.

In addition, the CO₂ adsorption amount was also calculated by CO₂-TPD measurement, which is called stable CO₂ adsorption amount in this study. These results are summarized in Table 1 and Table S2 including the signal areas of FT-IR spectra of CO₂ adspecies (Fig. 1 (I)). The equilibrium CO₂ adsorption amount increased with increasing the CO₂ concentration from 0.04 vol% to 1 vol% in the presence and absence of water (Table S2, entries 1–6), which is a similar tendency to the adsorption area of FT-IR measurement (The adsorption of CO₂ in the presence of water vapor is discussed later.). However, the amount of stable CO₂ adsorption amount is almost the same at each CO₂

Table 1

Summary of CO₂ adsorption amount and water adsorption amount.

Entry	Gas		Sample amount /g	TPD measurement (303–873 K)	
	CO ₂ concentration /vol%	Water vapor /vol%		Stable CO ₂ adsorption amount /mmol g ⁻¹	H ₂ O amount /mmol g ⁻¹
1	0.04	~0	0.3	0.12	0.15
2	0.1	~0	0.3	0.12	0.28
3	1	~0	0.3	0.12	0.09
4	0.04	0.85	0.12	0.14	1.00
5	0.04	1.6	0.12	0.14	0.91
6	1	0.85	0.12	0.14	1.06
7	0	0.85	0.12	-	1.02

Fig. S8

concentration, indicating that CO₂ is effectively adsorbed on CeO₂ at any CO₂ concentration. From these results, the larger FT-IR signal area under higher CO₂ concentration (Fig. 3) can be explained by the increase in the equilibrium CO₂ adsorption amount.

As mentioned above, low concentration of CO₂ can be adsorbed on CeO₂ and typical four main CO₂ adspecies can be observed, such as bidentate carbonate, hydrogen carbonate, monodentate carbonate, and polydentate carbonate, which are similar to the CO₂ adspecies on CeO₂ at high CO₂ concentrations. The adsorption efficiency of low concentration of CO₂ on CeO₂ is comparable or high compared with that of high CO₂ concentration. The stable CO₂ adsorption amounts under different CO₂ concentrations are almost the same, while the equilibrium CO₂ adsorption amounts are higher at higher CO₂ concentrations.

3.3. The effect of water vapor on CO₂ adsorption state over CeO₂

The effect of water vapor on the adsorption of CO₂ is important because the actual atmosphere contains at least several hundred ppm of water vapor. At first, the effect of water vapor on the adsorption of CO₂ on CeO₂ was investigated. CO₂ including water vapor (0.03 vol%, 1% humidity) was introduced into CeO₂, and the adspecies were measured by FT-IR (Fig. 5). Up to 30 min (Fig. 5(a)-(c)), the formation of typical CO₂ adspecies such as bidentate carbonate (1297 and 1570 cm⁻¹), polydentate carbonate (1360 cm⁻¹ and 1471 cm⁻¹), monodentate carbonate (1360 and 1508 cm⁻¹), and hydrogen carbonate (1217, 1391 and

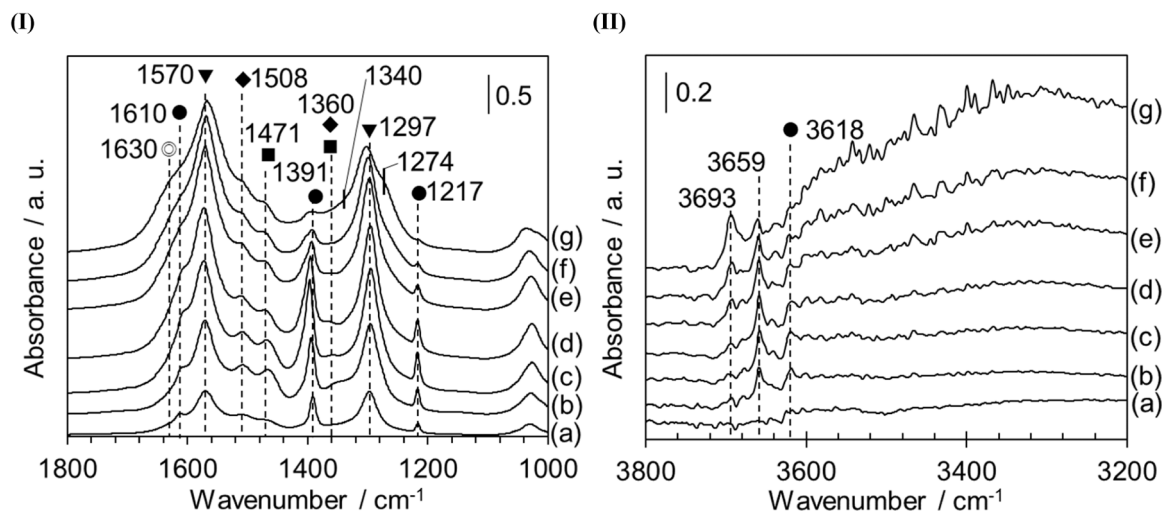


Fig. 5. FT-IR spectra of CO₂ and water adspecies on CeO₂ under 0.04 vol% CO₂/He with water vapor (0.03 vol%). (I) The spectra at 1000–1800 cm⁻¹ after 10 min (a), 20 min (b), 30 min (c), 40 min (d) 50 min (e), 60 min (f), and 90 min (g). (II) The spectra at 3200–3800 cm⁻¹ at the conditions of (I). Measurement conditions: CeO₂ 60 mg, disk size ϕ 20, rt, gas flow rate (CO₂ + He + water vapor) 30 mL/min.

1610 cm⁻¹) was observed. However, at longer times, the signal due to the hydrogen carbonate adspecies (1217, 1392, and 1610 cm⁻¹) decreased, and new absorption signals (1630, 3693, and around 3300 cm⁻¹), which are due to the adsorbed water molecule on CeO₂, were observed and increased with the time (Fig. 5(d)–(g)). On the other hand, the bidentate carbonate adspecies were not changed, suggesting that the bidentate carbonate adspecies on CeO₂ are stable in the presence of water vapor. New shoulder signals around 1297 cm⁻¹ (1274, and 1340 cm⁻¹) were also observed and increased with time. To check the signals due to water adspecies on CeO₂, only water vapor (0.3 vol% in He) was introduced into CeO₂, and the FT-IR spectrum of water adspecies was measured (Fig. S9). Only a broad signal around 1630 cm⁻¹ was observed in the range of 1000–1800 cm⁻¹, which is assignable to water adspecies on CeO₂, and there is no signal around 1297 cm⁻¹. These results suggest that the shoulder signals around 1297 cm⁻¹ in Fig. 5 is new CO₂ adspecies, which will be formed in the presence of water vapor. It was first confirmed that the hydrogen carbonate adspecies on CeO₂ were converted by water vapor to the new CO₂ adspecies similar to bidentate carbonates based on the time-course of CO₂ adsorption on CeO₂.

Stable CO₂ adsorption amount in the presence of water vapor was measured by CO₂-TPD measurement, and the results are shown in entries 4–6 in Table 1. The stable CO₂ adsorption amount in the presence of water vapor is estimated to be 0.14 mmol g⁻¹ at any water concentrations (0.85 and 1.6 vol%), which is about 1.2-fold higher than that in the absence of water vapor (0.12 mmol g⁻¹, entries 1–3). On the other hand, the equilibrium CO₂ adsorption amount, which was determined by the breakthrough measurement, depends on the CO₂ concentrations but was not so influenced by water vapor concentrations (Table S2, entries 1–6). These results indicate that water vapor promotes the adsorption of CO₂ on CeO₂, which tendency is different from that in the previous report [79]. Fig. 6 (I) shows the CO₂-TPD profile in the case of 0.04 vol% CO₂ with and without water vapor. In the absence of water vapor, both weakly adsorbed CO₂ (300–500 K) and strongly adsorbed CO₂ (500–873 K) were clearly observed. In contrast, in the presence of water vapor, weakly adsorbed CO₂ was mainly observed, and strongly adsorbed CO₂ was hardly done. The amount of the weakly adsorbed CO₂ largely increased by the presence of water, leading to the increase of the stable CO₂ adsorption amount (0.12 to 0.14 mmol g⁻¹) as discussed

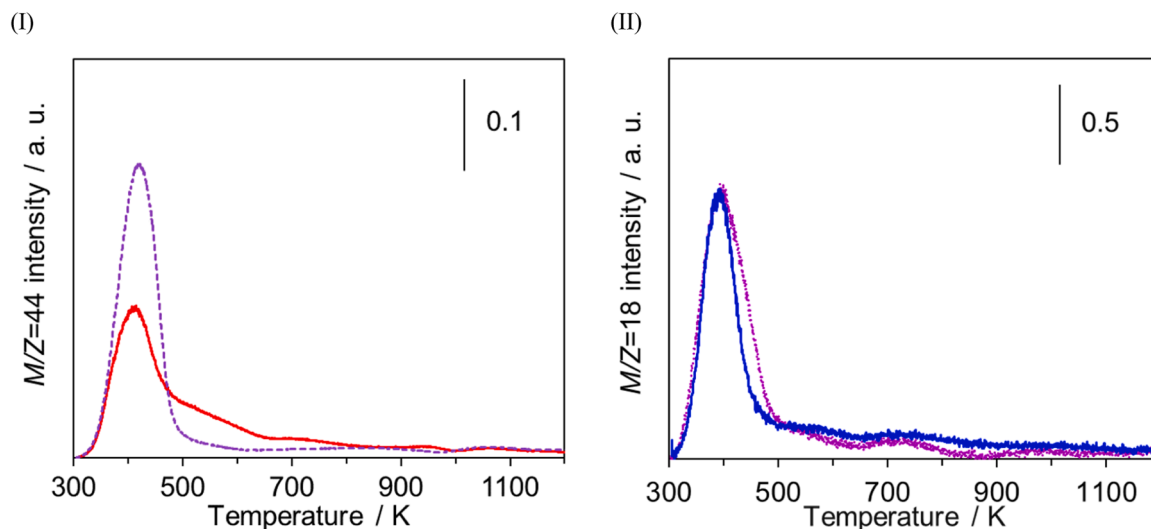


Fig. 6. CO₂- and H₂O-TPD over CeO₂. (I) CO₂-TPD over CeO₂ after the introduction of 0.04 vol% CO₂/He (red line) and 0.04 vol% CO₂/He with water vapor (0.85 vol%) (purple dash line). (II) H₂O-TPD over CeO₂ after the introduction of He with water vapor (blue line) and 0.04 vol% CO₂/He with water vapor (0.85 vol%) (purple dash line). Measurement conditions: CeO₂ 300 mg (100–150 μm grain), adsorption temperature rt, gas flow rate (CO₂ + He + water vapor) 30 mL/min.

above. These results suggest that new weakly CO₂ adspecies were formed over CeO₂ in the presence of water. Moreover, H₂O-TPD was also conducted to study the effect of CO₂ on water adsorption on CeO₂ (Fig. 6 (II)). The H₂O-TPD profiles are similar with and without CO₂, and the adsorption amount of water is also similar (Table 1, entries 6 and 7). These results indicate that water is comparatively strongly adsorbed on CeO₂, and that the adsorption is not so inhibited by CO₂ adsorption. Considering the water adsorption amount (1.0 mmol g⁻¹, Table 1) is similar to the surface Ce amount of CeO₂ (~1.1 mmol g⁻¹), the water layer will cover CeO₂. The new weakly adsorbed CO₂ will be adsorbed on the water layer via hydrogen bonding, which is responsible for the increase of CO₂ adsorption amount.

The adsorption strength of CO₂ and water molecules on the CeO₂ surface was investigated by DFT calculations. The CeO₂(111) surface was employed for this investigation since it represents the majority of highly crystallized CeO₂ nanoparticle surfaces due to its lowest surface energy. Four types of adsorption structures have been reported for a CO₂ molecule on the CeO₂(111) surface as described above: monodentate, bidentate, polydentate, and molecular adsorption. The adsorption energies of these structures were calculated to be -0.78, -0.53, -0.66, and -0.27 eV for monodentate, bidentate, polydentate, and molecular adsorption, respectively (see Fig. 7 for each structure). The monodentate structure (Fig. 7(a)) represents the strongest adsorption among these configurations, which is consistent with the previous reports of theoretical calculations [66,76,80,81]. In this structure, both of the two oxygen atoms belonging to CO₂ interact with the surface Ce atoms. The bidentate structure (Fig. 7(b)) involves the interaction between one of the oxygen atoms of CO₂ and the surface Ce atom, and the adsorption energy is weaker than that of the monodentate structure. The

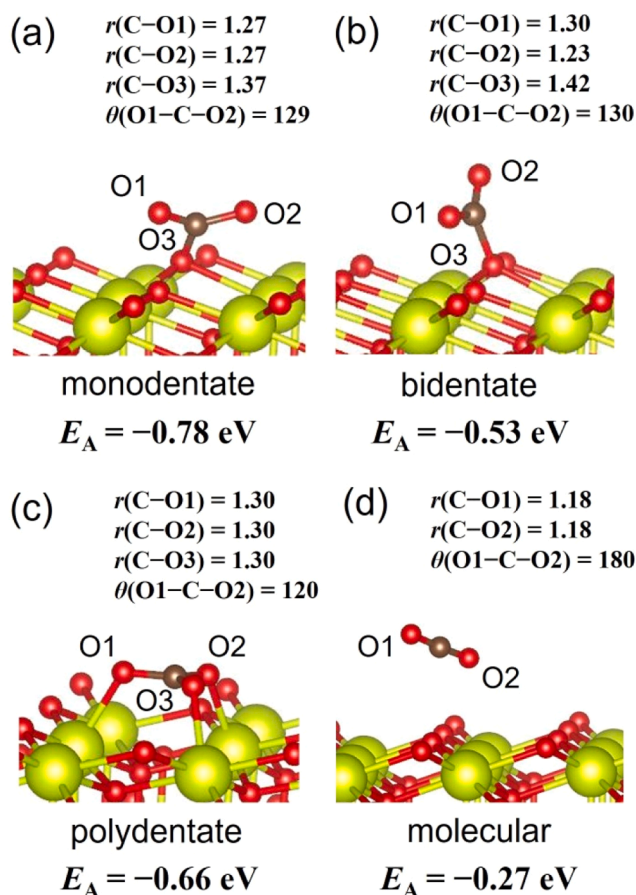


Fig. 7. Adsorption structures of a CO₂ molecule: (a) monodentate, (b) bidentate, (c) polydentate, and (d) molecular adsorption. C–O bond lengths and O–C–O angles are given in Å and degrees, respectively.

polydentate structure (Fig. 7(c)) involves a surface oxygen atom, which is translocated from its original surface position, and this adsorption structure is relatively stable. In the monodentate, bidentate, and polydentate structure, the C–O bond lengths are increased to 1.23 – 1.30 Å, compared to the gas-phase value of 1.18 Å. Also, the O–C–O angles were calculated to be 129, 130, and 120 degrees for monodentate, bidentate, and polydentate structures, respectively, indicating the strong activation of CO₂ molecule. On the other hand, the molecular adsorption (Fig. 7(d)) is relatively weak and involves only the acid-base interaction between one of the oxygen atoms of CO₂ and the surface Ce atom with an adsorption energy of -0.27 eV. Meanwhile, the adsorption energies of a water molecule on the CeO₂(111) surface were found to be -0.68 and -0.69 eV for molecular and dissociative adsorption, respectively (see Fig. S10 for structures). Given that the adsorption energy of the monodentate structure for CO₂ is -0.78 eV, the adsorption of CO₂ and water molecules exhibits a comparable strength.

The co-adsorption structures of CO₂ and water molecules were next examined. After a thorough investigation of possible structures, the most and second most stable co-adsorption structures are shown in Fig. 8, where the adsorption energies were calculated to be -1.49 and -1.33 eV, respectively. The hydrogen bond is formed between the CO₂ and water molecules, and the CO₂ molecule exhibits a bidentate structure. Considering that the sum of the adsorption energies of the most stable structures of CO₂ (monodentate) and water (dissociative) is -1.47 eV and that of CO₂ (bidentate) and water (dissociative) is -1.22 eV, the co-adsorption of CO₂ and water is feasible. The O–C–O angles and C–O bond lengths are similar to those of CO₂ adspecies without water (Figs. 7 and 8), suggesting that water vapor has little influence on the activation of CO₂. We also found several hydrogen carbonate species after the migration of proton or hydroxide ions from water to the adsorbed CO₂ molecules. The adsorption energies of the most stable structures are shown in Fig. S11, where the adsorption energies of both structures were -1.27 eV. One of the structures involves a hydrogen bond between the oxygen atom of hydrogen carbonate and the surface hydroxy group, and the other one involves the bidentate structure where two oxygen atoms interact with the surface Ce atoms. The adsorption energies of these structures are also comparable to those of co-adsorption structures (Fig. 8), which supports the co-existence of hydrogen carbonate species in experiments. The other possible structures are summarized in Fig. S12. As above, the adsorption energies of water and CO₂ on the CeO₂ surface are comparable, and the co-adsorption of CO₂ and water on CeO₂ is easier than the separate adsorption of CO₂ and water. Therefore, water and CO₂ do not hinder each other's adsorption. These results are also consistent with the results of FT-IR and mass spectroscopies.

Finally, the effect of water vapor on CO₂ adspecies on CeO₂ was studied. Water vapor (0.03 vol%, 1% humidity) was introduced to the

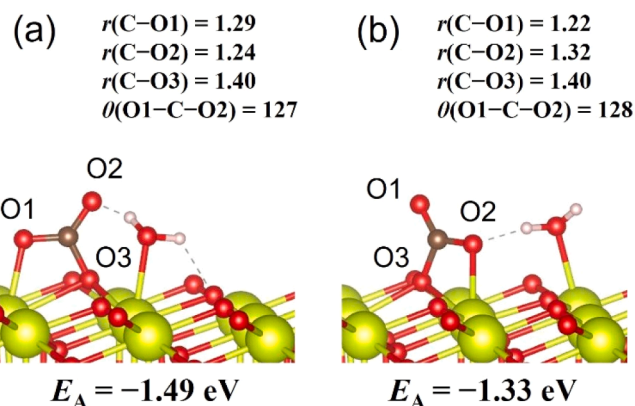


Fig. 8. Co-adsorption structures of CO₂ and water molecule. C–O bond lengths and O–C–O angles are given in Å and degrees.

CO₂-adsorbed CeO₂, and the CO₂ and water adspecies on CeO₂ were measured by FT-IR (Fig. 9). CO₂-adsorbed CeO₂ was prepared beforehand by the introduction of 0.04 vol% CO₂/He into CeO₂ for 120 min. The similar CO₂ adspecies (bidentate carbonate: 1293 and 1570 cm⁻¹, polydentate carbonate: 1362 cm⁻¹ and 1465 cm⁻¹, monodentate carbonate: 1360 and 1508 cm⁻¹, hydrogen carbonate: 1217, 1392 and 1611 cm⁻¹) were observed during 30 min after the introduction of water vapor (Fig. 9(I)-(a)-(e)). However, the signals due to the hydrogen carbonate species (1217, 1392, and 1611 cm⁻¹) decreased with time and completely disappeared at 60 min (Fig. 9(I)-(f)). The absorption signals (1630, 3693, and around 3300 cm⁻¹) due to water adspecies on CeO₂ were observed and increased with time, and the shoulder signals around 1293 cm⁻¹ (1277, and 1347 cm⁻¹) were observed and increased with time, which tendency is similar to the above case (Fig. 5). In order to check the desorption of CO₂ adspecies on CeO₂ by water vapor, water vapor was introduced into CO₂-adsorbed CeO₂, and the desorbed species were measured by mass analysis. Fig. 10 shows the amount of CO₂ and water in the outlet gas as a function of time. At the initial time, water (*M/Z* = 18) was not detected, however, the amount gradually increased as the time increased. CO₂ (*M/Z* = 44) was not detected at all the measurement time. These results indicate that water was adsorbed on CeO₂ at the initial time and CO₂ adspecies on CeO₂ were not desorbed by water vapor, which result does not contradict the DFT calculations. Considering the result of FT-IR analysis (Fig. 9), the disappearance of the hydrogen carbonate adspecies observed around 1400 cm⁻¹ is owing not to the desorption of the adspecies, but to the change of the adsorption state by the interaction with water molecules. The regeneration of the hydrogen carbonate adspecies on CeO₂ was also confirmed by heating the CO₂- and water-adsorbed CeO₂ sample from 298 to 463 K (Fig. S13), which also supports that the state of the hydrogen carbonate adspecies was changed by the interaction with water vapor.

From the above results, the adsorption image of CO₂ and water on CeO₂ in the case of a low concentration of CO₂ is shown in Fig. 11. On-top and bridged OH groups exist on the surface of CeO₂. In the absence of water vapor, bidentate and hydrogen carbonate adspecies are mainly formed by the introduction of CO₂ to CeO₂, and the hydrogen carbonate adspecies are formed by the reaction of CO₂ and an on-top OH group on CeO₂, not a bridged OH group. In the presence of water vapor, both water and CO₂ are adsorbed on CeO₂, and a larger amount of water than CO₂ exists on CeO₂. The bidentate carbonate adspecies are stable in the presence of water vapor, however, the hydrogen carbonate adspecies are not stable and change to a different state by the hydrogen bonding with water. CO₂ is adsorbed on CeO₂ and also on water adspecies of CeO₂ via hydrogen bonding, leading to a larger CO₂ adsorption amount than the case in the absence of water vapor.

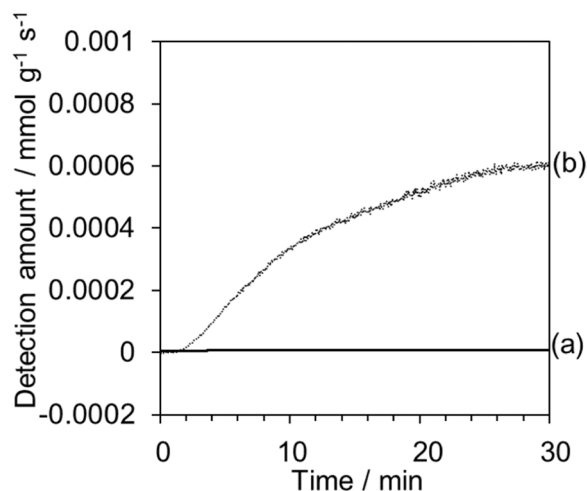


Fig. 10. The time-course of the CO₂ and H₂O amount in the outlet by the introduction of He with water vapor (0.85 vol%) into CO₂-adsorbed CeO₂. (a) CO₂ amount (*M/Z* = 44) and (b) H₂O amount (*M/Z* = 18). Measurement conditions: CeO₂ 1.0 g (100–150 μm grain), rt, gas flow rate (He + water vapor) 30 mL/min.

4. Conclusion

The adsorption behavior of low concentration of CO₂ on CeO₂ was investigated by *in situ* FT-IR and mass spectroscopy. The low concentration of CO₂, even atmospheric CO₂ (0.04 vol%), can be easily adsorbed on CeO₂, providing the main four CO₂ adspecies, bidentate carbonate, hydrogen carbonate, monodentate carbonate, and polydentate carbonate adspecies, that are similar to those observed with a high concentration of CO₂. The stable CO₂ adsorption amounts on CeO₂ with different concentrations of CO₂ are similar (~0.12 mmol g⁻¹), although the equilibrium CO₂ adsorption amounts increased with increasing CO₂ concentrations. Moreover, based on the breakthrough measurement, the adsorption efficiency of a low concentration of CO₂ is also high compared with that of a high concentration of CO₂, suggesting a high potential of CeO₂ as the CO₂ absorbent from the air.

The influence of water vapor on the CO₂ adsorption on CeO₂ was also studied by *in situ* FT-IR and mass spectroscopy. Water vapor changed the adsorption state of hydrogen carbonate adspecies via hydrogen bonding, and the stable CO₂ adsorption amount on CeO₂ is higher than that in the absence of water vapor. Based on DFT calculations, the adsorption strength of water and CO₂ are comparable, and CO₂ and water can co-exist because the co-adsorption is stronger via hydrogen bonding than

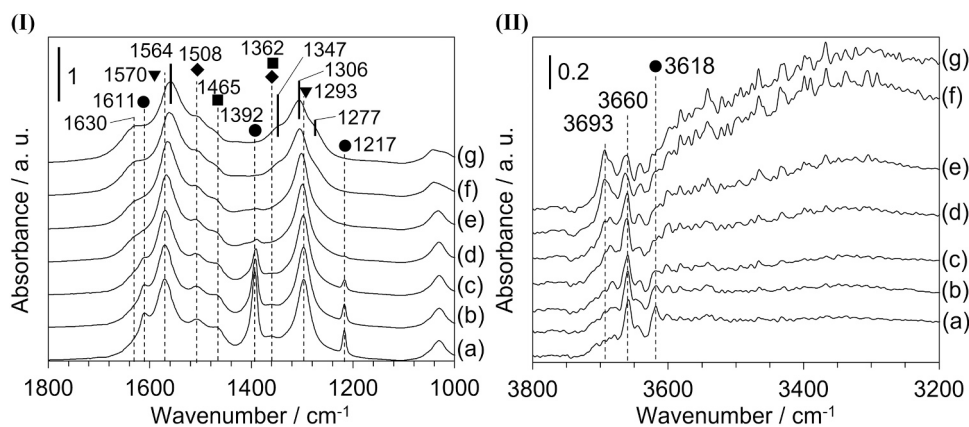


Fig. 9. FT-IR spectra of CO₂ and water adspecies on CeO₂ by the introduction of water vapor (0.03 vol%) into CO₂-adsorbed CeO₂. (I) 1000–1800 cm⁻¹ and (II) 3200–3800 cm⁻¹. (a) 0 min, (b) 5 min, (c) 10 min, (d) 20 min, (e) 30 min, (f) 60 min and (g) 90 min. Measurement conditions: CeO₂ 60 mg, disk size ϕ20, rt, gas flow rate (CO₂ + He + water vapor) 30 mL/min.

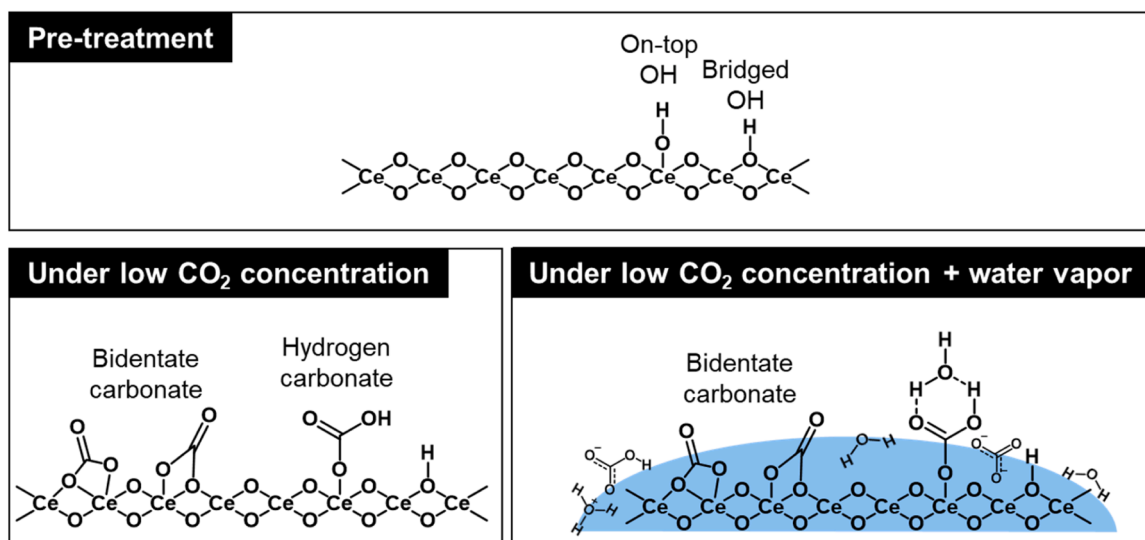


Fig. 11. CO₂ adsorption image with low CO₂ concentration on CeO₂ with and without water vapor.

that of the separative adsorption of CO₂ and water. The adsorbed water on CeO₂ can interact with additional CO₂ via hydrogen bonding, leading to the increase of CO₂ adsorption amount.

CRediT authorship contribution statement

Masato Akatsuka: Writing – review & editing, Formal analysis, Investigation. Akira Nakayama: Formal analysis, Investigation. Masazumi Tamura: Funding acquisition, Conceptualization, Supervision, Formal analysis, Writing – review & editing.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data Availability

Data will be made available on request.

Acknowledgments

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Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at [doi:10.1016/j.apcatb.2023.123538](https://doi.org/10.1016/j.apcatb.2023.123538).

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